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B.E./ B. TECH.DEGREE EXAMINATIONS, MAY 2024

Third Semester

CH22301 – CHEMICAL PROCESS CALCULATIONS*(Chemical Engineering)***(Regulation 2022)*****(USE OF PSYCHROMETRIC CHART IS PERMITTED)*****TIME:3 HOURS****MAX. MARKS: 100**

COURSE OUTCOMES	STATEMENT	RBT LEVEL
CO 1	Interpret the data presented in different unit systems and apply various gas laws to calculate the unknowns in a given system	3
CO 2	Build basic knowledge on various unit operations and processes and perform material balances for steady and unsteady state chemical systems.	3
CO 3	Provide insight into the concepts and calculations associated with gases which involves two phase systems.	3
CO 4	Perform energy balance calculations for steady and unsteady state chemical processes.	4
CO 5	Implement various methods used for analyzing combustion process and demonstrate the ability to understand process simulators.	4

PART- A (20x2=40Marks)

(Answer all Questions)

	CO	RBT LEVEL
1. Calculate the volume of 15 kg of Chlorine at a pressure of 0.9 bar and 293 K.	1	3
2. Differentiate Molarity and Normality.	1	2
3. State Dalton's law.	1	2
4. Define: Vapour Pressure.	1	2
5. Identify the limiting reactant and excess reactant when 12 kg of Carbon reacts with 32 kg of Oxygen to form Carbon-di- Oxide.	2	3
6. In an evaporator a dilute solution of 4% NaOH is concentrated to 25% NaOH. Calculate the evaporation of water per kg of feed.	2	3
7. SO ₂ is produced by the reaction between copper and sulphuric acid. How much Cu must be used to get 10 kg of SO ₂ ?	2	3
8. Mention the significance of Recycling operation.	2	2
9. Relate absolute humidity and molal humidity.	3	2
10. Define: Saturation.	3	2
11. Cite the difference between wet bulb temperature and dry bulb temperature.	3	2
12. Annotate the significance of psychrometric chart.	3	2

13.	State Kopp's rule.	4	2
14.	Differentiate specific heat and latent heat.	4	2
15.	Write the unsteady state energy balance equation for a batch reactor.	4	2
16.	Define: Theoretical flame temperature.	4	2
17.	Relate GCV and NCV.	5	2
18.	List any two process simulators.	5	2
19.	Highlight the importance of ultimate analysis.	5	2
20.	Give the applications of ORSAT analysis.	5	2

PART- B (5x 10=50Marks)

		Marks	CO	RBT LEVEL
21.(a)	Chimney gas has the following composition: CO ₂ : 9.5%, CO : 0.2%, O ₂ : 9.6% and N ₂ : 80.7%. Using ideal gas law, calculate: (a) its weight percentage (b) volume occupied by 0.5 kg of gas at 30 °C and 760 mm Hg. (c) density of the gas in kg/m ³ at condition of (b) (d) specific gravity of the gas mixture. (Density of air may be taken as 1.3 g/cc)	(10)	1	3
	(OR)			
(b)	A solution of caustic soda in water contains 20% NaOH by weight. The density of the solution is 1196 kg/m ³ . Find the molarity, normality and molality of the solution.	(10)	1	3
22.(a)	The waste acid from a nitrating process contains 23% HNO ₃ ; 57% H ₂ SO ₄ ; 20% water. This acid is to be concentrated to 27% HNO ₃ , 60% H ₂ SO ₄ by addition of 93% H ₂ SO ₄ and 90% HNO ₃ . Calculate the weight of acids needed to obtain 1000 kg of desired acid.	(10)	2	3
	(OR)			
(b)	Pure CO ₂ may be prepared by treating limestone with sulphuric acid. The limestone used in the process contains CaCO ₃ , MgCO ₃ and inert compounds. The acid used contains 12% H ₂ SO ₄ by weight. The residue from the process had the following composition: CaSO ₄ : 8.56%, MgSO ₄ : 5.23%, H ₂ SO ₄ : 1.05%, Inert : 0.53%, CO ₂ : 0.12%, H ₂ O : 84.51%. During the process, the	(10)	2	3

mass was warmed where CO₂ and H₂O got removed.

Calculate the following:

(a) The analysis of limestone

(b) The % excess acid used

23.(a) Air at a temperature of 20°C and pressure 750 mm Hg has a relative humidity of 80%. (10) 3 3

(a) Calculate the molal humidity of air.

(b) Calculate the humidity of this air if its temperature is reduced to 10°C and its pressure increased to 35 psi, condensing out some of the water.

(c) Calculate the weight of water condensed from 1000 ft³ of gas.

(d) Calculate the final volume of wet air leaving.

Data: Vapour pressure of H₂O at 20°C = 17.5 mm Hg and at 10°C = 9.2 mm Hg.

(OR)

(b) An air (B)-water (A) sample has a dry bulb temperature of 50 °C and a wet bulb temperature of 35 °C. Estimate its molal humidity, partial pressure of water, percentage humidity, humid heat and the relative saturation at a total pressure of 1 atm. Molecular weight of air = 28.84 (10) 3 3

24.(a) A natural gas has the following composition on mole basis: CH₄ – 84 %, C₂H₆ – 13 % and N₂ – 3 %. Formulate an empirical expression for heat to be added and calculate the heat to be added to raise the temperature of 10 kmol of natural gas from 298 K to 523 K using heat capacity data given below. (10) 4 3

$C_p^\circ = a + bT + cT^2 + dT^3$, kJ/kmol.K

Gas	A	b x 10 ³	c x 10 ⁶	d x 10 ⁹
CH ₄	19.2494	52.1135	11.973	-11.3173
C ₂ H ₆	5.4129	178.0872	-67.3749	8.7149
N ₂	29.5909	-5.141	13.1829	-4.968

(OR)

(b) Dry methane and dry air at 298 K and 1 bar pressure are burnt with 100% excess air. The standard heat of reaction is –802 kJ/g mole of methane. (10) 4 3

Determine the final temperature attained by the gaseous products if combustion is adiabatic and 20% of heat produced is lost to the surroundings.
 Data: C_{pm} values (J/g mole K) for the components are: O_2 : 31.9, N_2 : 32.15, H_2O : 40.19, CO_2 : 51.79.

- 25.(a)** The Orsat analysis of the flue gases from a boiler house chimney gives **(10)** **5** **3**
 CO_2 :11.4%, O_2 :4.2% and N_2 :84.4% (mole %). Assuming that complete combustion has taken place, (a) Calculate the % excess air, and (b) Analyze the C:H ratio in the fuel.

(OR)

- (b)** The ultimate analysis of a coal sample is given as C – 61.5%, H_2 – 3.5%, S – **(10)** **5** **3**
 0.4%, Ash 14.2%, N_2 – 1.8% and rest oxygen. Calculate the theoretical oxygen requirement per unit weight of coal and the Orsat analysis of flue gases, if coal is burnt with 90% excess air.

PART- C (1x 10=10Marks)

(Q.No.26 is compulsory)

- | | Marks | CO | RBT
LEVEL |
|---|-------------|----------|--------------|
| 26. The average molecular weight of a flue gas sample is calculated by two different engineers. One engineer used the correct molecular weight of N_2 as 28, while the other used an incorrect value of 14. They got the average molecular weight as 30.08 and the incorrect one as 18.74. Calculate the % volume of N_2 in the flue gases. If the remaining gases are CO_2 and O_2 calculate their composition also. Evaluate the error percentage of the faulty calculation. | (10) | 1 | 5 |
