Q. Code:237907

Reg. No.

B.E / B.TECH. DEGREE EXAMINATIONS, MAY 2024 Sixth Semester

CH18604 – PROCESS EQUIPMENT DESIGN I

(Chemical Engineering)

(Regulation 2018/2018A)

(HEAT AND MASS TRANSFER HANDBOOK AND STANDARD CHARTS ARE ALLOWED)

TIME: 3 HOURS

MAX. MARKS: 100

- **CO1** Impart knowledge on the importance of design information and data.
- CO 2 Identify the methods of process design of separation columns.
- CO 3 Impart the basics of process design of heat transfer equipment's.
- CO 4 Outline the essentials of fluid movers and related items.
- CO 5 Evaluate the concepts of piping and instrumentation diagram and site selection.

PART- A (10 x 2 = 20 Marks)

(Answer all Questions)

		CO	RBT LEVEL
1.	Write the significance of having control over Design information and data.	1	1
2.	Distinguish the types of prediction methods of any extensive property of a given sample.	1	3
3.	Sketch the graphical representation of different possible feed conditions that can feed into a binary distillation column?	2	2
4.	Sketch the schematic of a flash column used for representing a binary mixture separation.	2	2
5.	A hot fluid at 100°C enters a heat exchanger at a mass flow rate of 14kg/hr. Its specific heat is 2000 J/kg-K. It is to be cooled by another fluid entering at 25°C with a mass flow rate 25 kg/hr and specific heat 400 J/kg-K. The overall heat transfer coefficient based on outside area of 2.5m ² is 250W/m ² K. Find the exit temperature of the hot fluid when the fluids are flowing counter current.	3	3
6.	Sketch the Temperature profile for a plate type heat exchanger, with proper assumptions.	3	2
7.	List the guidelines for the control valves in the pump design.	4	2

8. Rank the different types of valves based on pressure drop. 4 2

- 9. Differentiate safety valves and rupture disc.
- 10. Calculate the optimum pipe diameter for a water flow rate of 12 kg/s. Carbon steel pipe 5 3 shall be used.

PART- B (5 x 14 = 70 Marks)

		Marks	CO	RBT LEVEL
11. (a)	(i) Elucidate with example the best way to design the pipe network	(7)	1	3
	system for your apartment/home, justify your assumptions.			
	(ii) Illustrate with example the accuracy of design data and their	(7)	1	3
	sensitivity in process equipment design.			
	(OR)			
(b)	Estimate the important fluid properties of the main component of LPG. List	(14)	1	3
	the assumptions if any. Following relevant data base can be used with			
	assumptions.			
12. (a)	A plant with an annual through put of 0.09 million tonnes requires a	(14)	2	3
	distillation column to separate an equimolar mixture of methanol in water			
	available at its boiling point. Design a sieve tray column and find the			
	number of actual plates for the operation at atmospheric pressure with a			
	reflux ratio of 1.5 times the minimum			
	Given:			

Overhead product – 93.2 mol% methanol Residue – 1.6 mol% methanol Avg. Liq. Density- 875 kg/m³ Vapour density at top – 2.85 kg/m³ Vapour density at bottom – 3.21 kg/m³ Avg. liquid Viscosity – 0.0003kg/m.s Top Column Temp. – 360.6 K Bottom Column Temp. – 379.6 K Tray spacing – 68cm Tray efficiency – 45% Vapour velocity in the column can be estimated by using Brown Sonder's eqn. 2

(14)

2

3

3

	Vapour velocity = $\frac{k_{v\sqrt{\rho_{L}-\rho_{v}}}}{\rho_{v}}$										
	kv=0.0428										
Χ	0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	1
Y	0	0.42	0.57	0.66	0.73	0.78	0.83	0.87	0.92	0.92	1
(OR)											

(b) Referring to the 3-component diagram in Figure given below, if 30,000 kg/h of Ternary mixture of 34 wt% of A, 19% of B, and 47% of C was fed into a decanter (a mixer and settler) operating at 25 °C, what would the flow rates of two liquid streams leaving the decanter be and comment of minimum solvent required?



13. (a) Estimate the reboiler process design parameters for steam on inside and (14) 3 3 outside 12 mm & 18mm vertical tube of 2.5m long. The steam generating rate is 0.035kg/s per tube and the boiling take place at 4.2 bar. Density of liquid and vapour are 922 and 2.12 kg/m³. Saturation temperature is 144° C. Thermal conductivity and Viscosity are 0.685 W/m° C & 95 x 10 ⁻⁶kg/m.s, NPr - 1.29.

(OR)

(b) Design 2 - 4 Shell and tube heat exchanger to process 47.5 kg/s of crude oil (14) 3 that's need to be heated from 298 K to 335 K by that heat exchanger with a bottom product in a distillation unit which is to be cooled from 460 K flowing at a rate of 29 kg/s. The physical properties of various streams at

mean temperature are given below.

Property	Crude oil	Bottom Product
Cp (kJ/kg K)	2.2	2.5
μ (kg/m-s)	3.2x10 ⁻³	5.1x10 ⁻³
ρ (kg/m3)	810	870
K (W/m K)	0.162	0.115

Assume the relevant data for a feasible design.

14. (a) A pipeline connecting three tanks contains seven square elbows, a globe (14) 4 3 valve half open and gate valve fully open. The line is cast iron pipe, 25mm internal diameter, length 125 m. The properties of the fluid are : Viscosity is 0.9995 mNs/m², Density is 999kg/m³, Calculate the total pressure drop due to friction when the flow rate is 3700kg/h and give the inferences.

(OR)

- (b) A compressor to be used to draw nitrogen off of a cryogenic storage tank (14) 4 3 and boost the pressure to feed a plant processes. The flow requirement will vary throughout the 8 hour production day, but will average about 15 CFM. Suction pressure at 5psi and discharge pressure is 65 psi. Site: 1000 ft elevation, outdoors, Ambient 100°F Utilities: 460V / 3ph/ 60 Hz, 80°F fresh water Critical Pressure and temperature are 493 psia and 228° R Capacity: 20SCFM Design a proper compressor for the above given data.
- 15. (a) Choose an industry and suggest a suitable plant layout and site selection (14) 5 2 with a neat chart with involving environmental considerations.

(OR)

- (b) (i) Enumerate Automatic Control Schemes of distillation column used at (7) 5 2 process industries
 - (ii) As a chemical engineer, suggest your views on how PFD diagram is (7) 5 2 useful in process equipment design

<u>PART- C (1 x 10 = 10 Marks)</u>

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(Q.No.16 is compulsory)

16.

	Marks	CO	RBT LEVEL	
Design the solar water heater system for your hotel, assuming that 5 people	(10)	3	5	
will be using warm water at 55°C, with the total water capacity of				
250 litres/day and available heat flux is $0.8W/m^2$. Assume the missing				
parameters and list them and justify them.				
